

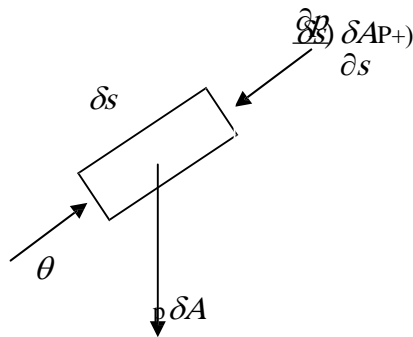
Fluid and fluid flow

Definitions

Fluid, laminar flow, turbulent flow, Boundary layer, Reynolds Number, adiabatic flow, steady flow, unsteady flow, Uniform flow, non-uniform flow, rotational flow, Irrotational flow, one dimension flow, two dimension flow, three dimension flow, stream line

Derivation of Eulers equation along a stream line

) assume a particle in a stream line, steady and frictionless flow the a force diagram 6Q can be written as



$$\rho g \delta A \delta s$$

$$\cos \theta = \frac{\delta z}{\delta s}$$

$$\sum F_s = m a_s$$

$$p \delta A - \left(p + \frac{\partial p}{\partial s} \delta s \right) \delta A - \gamma \delta A \delta s \cos \theta = \rho \delta A \delta s a_s$$

$$p \delta A - p \delta A - \frac{\partial p}{\partial s} \delta s \delta A - \gamma \delta A \delta s \cos \theta = \rho \delta A \delta s a_s \text{ dividing by } \delta A \delta s \text{ then}$$

$$-\frac{\partial p}{\partial s} = \gamma \cos \theta + \rho a_s$$

$$\text{But } a_s = v \frac{\partial v}{\partial s} \text{ for steady state flow}$$

$$\frac{\partial p}{\partial s} = -\rho g \cos \theta - \rho a_s$$

$$\frac{\partial p}{\partial s} + g \frac{\partial z}{\partial s} + v \frac{\partial v}{\partial s} = 0$$

Since s is the only dependent variable then

$$\frac{dp}{\rho} + g dz + v dv = 0$$

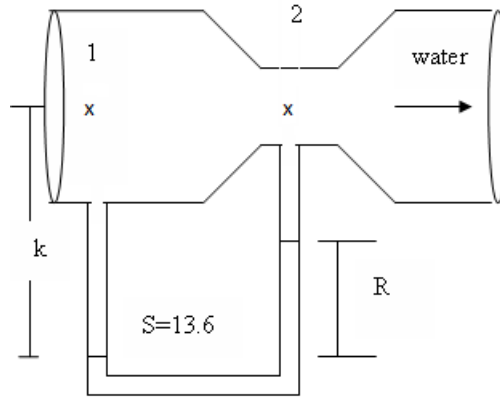
= constant) then This is Euler's equation and for incompressible flow (i.e

$$\frac{p}{\rho} + \frac{v^2}{2} + gz = \text{constant}$$

this is Bernoulli equation

continuity equation and its application (✓)
Application of Bernoulli equation (✓)

, derive an equation that relate the distance R and the velocity at 1 Ex. For the venturi meter shown in fig 3, what is the volume flow rate in m³/s if R=20 cm, D₁=20 cm and D₂=10 cm. If R=2 point



, neglect loss then 2 & 1 Bernoulli equation between

$$\frac{P_1}{\gamma_w} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\gamma_w} + z_2 + \frac{V_2^2}{2g} \quad (1 \text{ eq})$$

and $z_2 = z_1 + R$ becomes then eq(

$$\frac{P_1 - P_2}{\gamma_w} = \frac{V_2^2 - V_1^2}{2g} - R \quad (2 \text{ eq})$$

2 & 1 Pressure equation

$$P_2 + k\gamma_w - R S \gamma_w - (k + R)\gamma_w = P_1 \quad (3 \text{ eq})$$

Then

$$-R(S - 1)\gamma_w = P_2 - P_1 \quad (4 \text{ eq})$$

But from continuity equation

$$Q_1 = Q_2$$

$$A_1 V_1 = A_2 V_2 \quad (5 \text{ eq})$$

assume for incompressible flow $\rho_1 = \rho_2 = \rho$

$$A_1 V_1 = A_2 V_2 \Rightarrow V_2 = \frac{A_1}{A_2} V_1 \quad (6 \text{ eq})$$

$$\left(\frac{D_1}{D_2}\right)^2 V_1^2 = V_2^2 \quad (6 \text{ eq})$$

(4) = eq(2) eq(

$$\frac{P_1 - P_2}{\gamma_w} = -R(S - 1) - \frac{V_1^2}{2g} \left(\left(\frac{D_1}{D_2}\right)^2 - 1 \right)$$

then6 and using eq

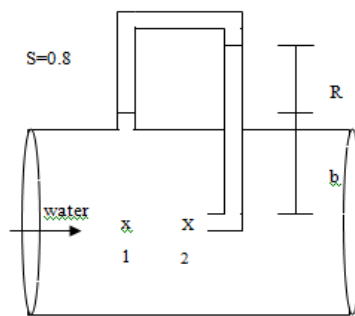
$$\left(\frac{V}{g} \right)^2 = \frac{1}{g^2} \left[\frac{1}{R} \left(\frac{4}{D} \right)^2 \frac{D}{g^2} \right]$$

$$V = \sqrt{\frac{(1gR(s-2))}{\left[\left(\frac{2}{D} \right)^4 \right]}}$$

$$V = \sqrt{\frac{(m/s \cdot 2.592) - 1 - 13.6 (0.02 \times 10 \times 2)}{\left(\frac{2}{0.1} \right)^4}}$$

$$\left(\pi \cdot 2.592 \right) = \frac{2D}{4} \left(\pi \cdot 2.592 A = 2 Q = V \frac{0.1^2}{4} \right) \text{ m / s } 0.02^2 =$$

& R1 Derive an equation that relate v



then2 &1 Applied Bern. Equation

$$\frac{V^2}{g^2} + \frac{p_1}{\gamma} + z_1 = \frac{V^2}{g^2} + \frac{p_2}{\gamma} + z_2$$

$$\frac{V^2}{g^2} + \frac{p_1}{\gamma} + z_1 = \frac{V^2}{g^2} + \frac{p_2}{\gamma} + z_2 \quad (1)$$

2and 1 For pressure equation between

$$p_1 + (k + a + R)\gamma_{water} - RS\gamma_{water} - a\gamma_{water} = p_2$$

$$-s) - k_1 = R \frac{P_1 P}{\gamma_{water}} \quad (2)$$

) then 2) = eq (1) eq (

$$\frac{V^2}{g^2} = R(s-1) \quad (3)$$

$$V_1^2 = \frac{D_1^2}{D_2^2} V_2^2 \quad (4)$$

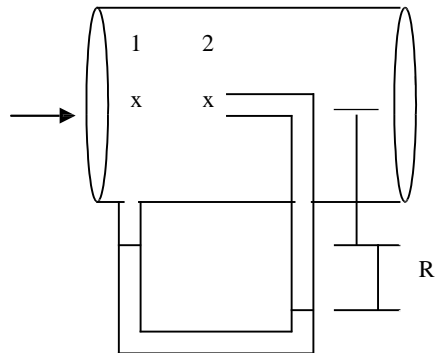
) then 3) INTO (4)

$$\frac{V_1^2}{g^2} = R(s-1) \frac{D_1^2}{D_2^2}$$

Then

$$V_1 = \sqrt{\frac{(1gR(s-2) + \frac{D_1^2}{D_2^2} V_2^4)}{[\frac{D_1^2}{D_2^2}]^2 - 1}} \quad \text{then } \frac{D_1^2}{D_2^2} R = \frac{V_1^2}{g^2} \text{ and}$$

1m what is the velocity at point 0.2 . If R=1 Derive a relation between R and v



, neglect loss then 2 & 1 Bernoulli equation between

$$\frac{P_1}{\gamma_w} + z_1 + \frac{V_1^2}{2g} = \frac{P_2}{\gamma_w} + z_2 + \frac{V_2^2}{2g} \quad (1eq)$$

$z_2 = z_1$ and $V_2 = V_1$) becomes then eq(

$$\frac{P_1 - P_2}{\gamma_w} = \frac{V^2}{g} \quad (2eq)$$

2.1 Pressure equation

$$P_2 + a\gamma_w + R S \gamma_w - (R + a)\gamma_w = P_1 \quad (3eq)$$

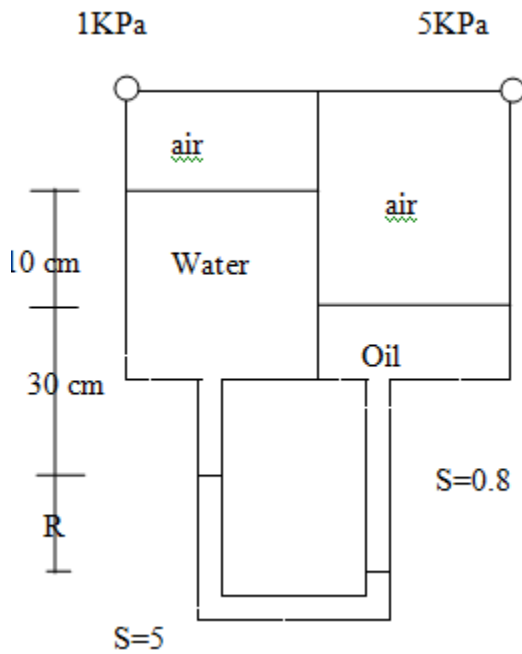
Then

$$P_2 - P_1 = (R + a - a - R S)\gamma_w \quad (4eq)$$

then $R = \frac{P_2 - P_1}{\gamma_w} + a - S a$

$$R = \frac{5000 - 1000}{9.8} + 0.4 - 0.8 \times 0.4 = 13.6 \text{ m} \quad (13.6 \text{ m})$$

Ex. What is the value of R



$$5000 = 0.3R\gamma_w - s_o\gamma_w(R + 1\gamma_w + s_o \cdot 0.4 + 1000)$$

$$\gamma_w 0.3 \times 0.8 \gamma_w + 0.4 - 1000 - 5000) R \gamma_w = 0.8 - 5)$$

$$\text{---} m 0.0571 = \frac{2400 + 4000 - 4000}{42000} R =$$